

Liquid Volume Fraction Model for Vapor-Liquid Surface Tension Data for the Binary Mixtures {Ar + Kr} and {CH₄ + Kr}

Lambert Van Poolen^{C, S}
Calvin College, Grand Rapids, MI, U.S.A.

Cynthia Holcomb
National Institute of Standards and Technology (retired), Boulder, CO, U.S.A.

A simple, unique method to correlate vapor-liquid surface tension data for binary mixtures of {Ar + Kr} and {CH₄ + Kr} is presented. For both mixtures, the data of Holcomb and Zollweg¹ are along eight isotherms that cover the liquid-vapor coexistence region below the critical pressures of each component. These data are correlated within their estimated experimental uncertainty of (0.2×10^{-3} N/m) along paths of fixed overall composition for component one (X_1) for which the liquid volume fraction (LVF) is fixed at a value of one-half ($1/2$) to assure access to the critical line of the mixture². This approach is motivated by the Van Poolen phase rule³ that accounts for system-intensive variables along with the phase-intensive variables of the Gibbs phase rule. The degrees of freedom given by the Van Poolen phase rule ($f = \{C + 1\}$ where C is number of components) is in this case = 3. In addition to the two system-intensive variables, X_1 and $LVF = 1/2$, the third variable is the phase-intensive variable temperature (T). Similar surface tension data of Nadler, et al.⁴, for the mixture {Ar + Kr} are also correlated using this method. The correlations of the two separate data sets indicate an offset of 0.1×10^{-3} N/m between them -- a value within experimental uncertainty. Mixture surface tension (σ) is represented by the equation (from the theory of critical behavior):

$$\sigma = \sigma_o \left[(T_c - T) / T_c \right]^\mu,$$

where σ_o is the surface tension coefficient and T_c is the critical temperature both given as a function of X_1 (for which $LVF = 1/2$), and μ is the non-classical scaling exponent = 1.26. The equations for σ_o and T_c each required one fitted constant. This equation correlates the surface tension data removed from the critical region while allowing for estimation of two-phase, binary-mixture surface tension in the critical region for which data were not available.

[1] C.D. Holcomb and J.A. Zollweg, *Fluid Phase Equilibria*, **75** 213 (1992).

[2] L.J. Van Poolen, C.D. Holcomb, and J.C. Rainwater, *Industrial and Engineering Chemistry Research*, **40** 4610 (2001).

[3] L.J. Van Poolen, *Fluid Phase Equilibria*, **58** 133 (1990).

[4] K.C. Nadler, J.A. Zollweg, W.B. Street and I.A. McLure, *Journal of Colloid and Interface Science*, **122** (2) 530 (1988).