

Water Solubility in N-Alkanes and Ethanol Mixtures for LLE Conditions Using the Polar GC-PC-SAFT EoS

Moustafa Mourah, Jean-Charles de Hemptinne^{C, S} and Nicolas Ferrando
IFP, Departement Thermodynamique et Simulation Moleculaire, Rueil-Malmaison Cedex, France

Jean-Philippe Passarello and Pascal Tobaly
LIMHP, CNRS UP13, Villeteuse, France

No consensus exists at this point on how to treat water with the polar GC-SAFT equation of state (Eos). Several authors have proposed methods for evaluating high pressure and high temperature phase envelopes of water containing mixtures [1-3]. Yet, none of them managed to determine correctly both solubilities (water in hydrocarbon and hydrocarbon in water). As a matter of fact, it has been shown that among the associating models, SAFT is not recommended for describing these two solubilities simultaneously [4, 5]. Recently, it has been shown how the number of parameters involved in the SAFT theories make it very difficult to identify unambiguously the parameters of a complex molecule such as water [6]. In this work, we have further investigated this issue, by including other type of data, as virial coefficients, or information concerning hydrogen bonding, and discussing the physical significance of the association parameters. This first investigation has led us to identify two sets of parameters that are further used for phase equilibrium calculations with alkanes, whose parameters are determined using Tamouza's group contribution method [7]. Both vapour-liquid as liquid-liquid equilibria are shown, and, using one set of parameters, can be predicted without binary interaction parameters. In mixture with ethanol, described according to NguyenHuynh et al. [8], cross-association is encountered. The cross-association combining rules are determined without interaction coefficients, and the ternary alkane-ethanol-water liquid-liquid system is predicted using an extrapolation for the ethanol-alkane binary interaction coefficient.

- [1] Galindo, A., Whitehead, P.J., Jackson, G. and Burgess, A.N., "Predicting the high-pressure phase equilibria of water plus n-alkanes using a simplified SAFT theory with transferable intermolecular interaction parameters", *Journal of Physical Chemistry*, Vol. 100, No. 16, 1996, pp. 6781-6792.
- [2] Li, X.S., Englezos, P., "Vapor-liquid equilibrium of systems containing alcohols, water, carbon dioxide and hydrocarbons using SAFT", *Fluid Phase Equilibria*, Vol. 224, No. 1, 2004, pp. 111-118.
- [3] Al-Saifi, N.M., Hamad, E.Z. and Englezos, P., "Prediction of vapor-liquid equilibrium in water-alcohol-hydrocarbon systems with the dipolar perturbed-chain SAFT equation of state", *Fluid Phase Equilibria*, Vol. 271, No. 1-2, 2008, pp. 82-93.
- [4] Economou, I.G., Tsonopoulos, C., "Associating models and mixing rules in equations of state for water-hydrocarbon mixtures", *Chem. Eng. Sci.*, Vol. 52, No. 4, 1997, pp. 511-525.
- [5] Economou, I.G., Donohue, M.D., "Equation of state with multiple associating sites for water and water-hydrocarbon mixtures", *Ind. Eng. Chem. Res.*, Vol. 31, No. , 1992, pp. 2388-2394.
- [6] Clark, G.N.I., Haslam, A.J., Galindo, A. and Jackson, G., "Developing optimal Wertheim-like models of water for use in Statistical Associating Fluid Theory (SAFT) and related approaches", *Molecular Physics*, Vol. 104, No. 22-24, 2006, pp. 3561-3581.
- [7] Tamouza, S., Passarello, J.P., Tobaly, P. and de Hemptinne, J.C., "Group contribution method with SAFT EOS applied to vapor liquid equilibria of various hydrocarbon series", *Fluid Phase Eq.*, Vol. 222-223, No. 2004, pp. 67-76.
- [8] NguyenHuynh, D., Passarello, J.P., Tobaly, P. and de Hemptinne, J.C., "Application of GC-SAFT EOS to polar systems using a segment approach", *Fluid Phase Equilibria*, Vol. 264, No. 2008, pp. 62-75.